

GAS FLOW RATE THROUGH FULL-OPEN CONTROL VALVE OR REGULATOR

Version 1.04 7 Feb 2005

Note: User must fill in shaded cells.

Plant Name:	
Location:	
Engineering Job No.	
Vessel / Equipment No.	
Service:	
Manufacturer:	
Model No.	
Nominal Size (Inches):	
Relief Device Designer:	

Input Data:

Upstream Pressure	P ₁	264.70	psia	
Downstream Pressure	P ₂	146.70	psia	
Upstream Temperature	T ₁	0.0	° C	
Gas Molecular Weight	MW	28.013		
Compressibility	Z	1.000		(See Notes Below)
<i>Provide two of the four valve parameters</i>				
Valve Flow Coefficient	C _v	60.00		
Valve Type Parameter	x _t	1.0		(See Notes Below)
Valve gas coefficient	C _g			
Fisher valve parameter	C ₁			

Results:

Valve Flow Coefficient	C _v	60.00	
Valve Type Parameter	x _t	1.0	
Upstream Temperature	T ₁	492.0	° R
Gas Density	ρ ₁	1.4046	lbs/ft ³
Difference Between P ₁ and P ₂	ΔP	118.00	psi
Valve Type Parameter X Upstream Pressure	x _t P ₁	264.70	psi
Pressure Drop Through Valve	ΔP _x	118.00	psi
Expansion Factor	Y	0.851	
Gas Flow Rate	W	41630.26	lbs/hr

Notes:

$\rho_1 = \frac{P_1 MW}{10.72 T_1}$ $\Delta P_x = \text{lesser of } \Delta P \text{ or } x_t P_1$ $Y = 1 - \frac{\Delta P_x}{3 x_t P_1}$ $W = 63.3 C_v Y \sqrt{\Delta P_x \rho_1}$ $C = C_v / C_1$	<table border="1"> <thead> <tr> <th>Valve Type</th><th>x_t</th></tr> </thead> <tbody> <tr> <td>Venturi Angle</td><td>0.2</td></tr> <tr> <td>90° Butterfly</td><td>0.2</td></tr> <tr> <td>60° Butterfly</td><td>0.5</td></tr> <tr> <td>Globe</td><td>0.9</td></tr> <tr> <td>Default</td><td>1.0</td></tr> </tbody> </table>	Valve Type	x _t	Venturi Angle	0.2	90° Butterfly	0.2	60° Butterfly	0.5	Globe	0.9	Default	1.0
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$$C_v = C_g / C_1$$

$$x_t = 0.00063 C_1^2$$

Xt

Using the default value (1.0) is conservative but **flow will never choke**.

If the Xt is 0.8 then the valve will choke when the pressure drops by 80%. If the Xt is 0.2 the valve will choke when the pressure drops by 20%.

Xt values are generally available in vendor literature

The rule-of-thumb value for Xt is 0.5. Note that this is not such a "safe" number to choose since this valve varies greatly depending on the style of valve. If you estimated a 0.5 valve and have a globe valve, for example, you are actually going to get much more flow than you estimated.

Z

Compressibility is a function of temperature and pressure. Note that the flow rate increases when the Z value is reduced from 1.0. So, to be conservative you need to estimate a low Z value of look it up by doing a quick SafSiz run (SafSiz reports this value).